

# High Fidelity Computational Analysis of CO<sub>2</sub> Trappings at Pore-scales

Project Number: DE-FE0002407

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U.S. Department of Energy  
National Energy Technology Laboratory  
Carbon Storage R&D Project Review Meeting  
Developing the Technologies and Building the  
Infrastructure for CO<sub>2</sub> Storage  
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# Presentation Outline

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- Benefit to the Program
- Project Overview
- Technical Status
  - Pore-network modeling
  - Conductance derivation for irregular geom.
  - Pore-to-CFD Computations
  - Paul M. Delgado's presentation "Stochastic Multiscale Modeling of Fluid Flow in Porous Media for CO2 Storage Applications"
- Accomplishments
- Summary

# Benefit to the Program

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- Identify the Program goals being addressed.
  - CO2 capacity assessments, simulation, and risk assessments
- Project benefits statement:

Increasing CO2 emissions to the atmosphere from the anthropogenic sources is expected to be the major cause undesirable Climate Change and Global warming trends of our planet. One method to mitigate this threat is to capture CO2 before releasing to the atmosphere and store it in the subterranean reservoirs (e.g., exhausted coal seams or oil fields) or utilize it for Enhanced Oil Recovery (EOR) or Methane Gas Recovery. However, the overall storage, leakage, and migration potential of CO2 within these reservoirs is not well understood. Due to the expense and risk involved with testing Carbon Capture Utilization & Storage (CCUS) technologies, it is crucial to simulate the flow of CO2 at the high fidelity. **This is achieved by computational investigation using semi-empirical variational calculus methods for computing flow conductance rule in single- and multi-phase systems and multi-scale framework for coupling the micro- and macro- scales.**

# Project Overview:

## Goals and Objectives

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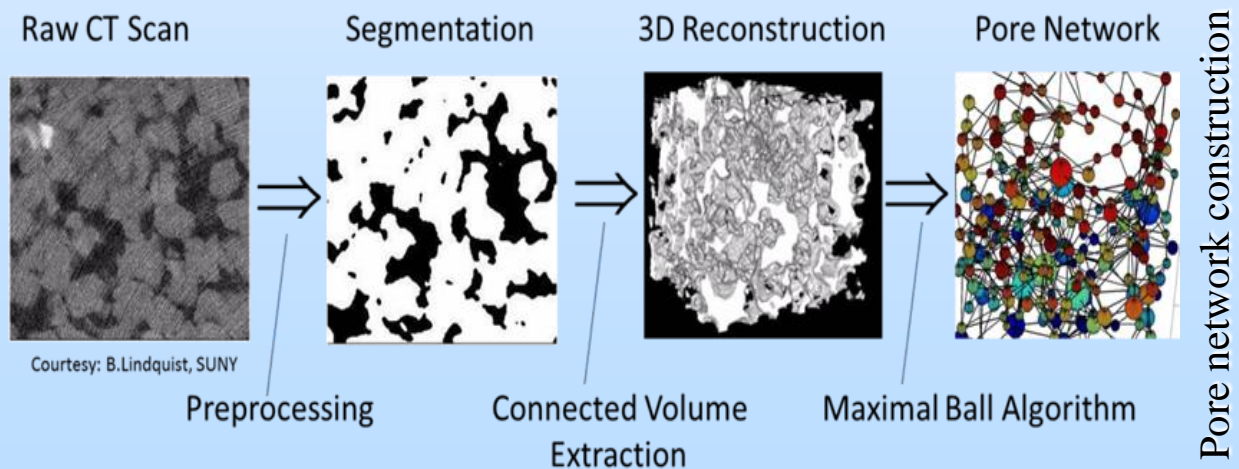
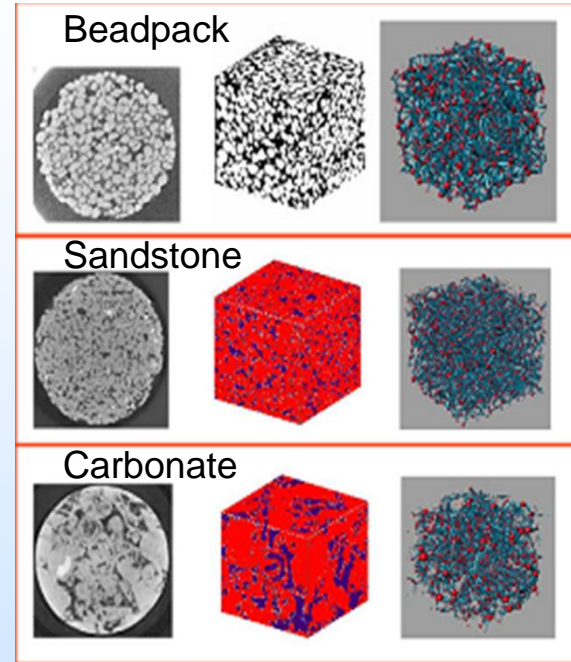
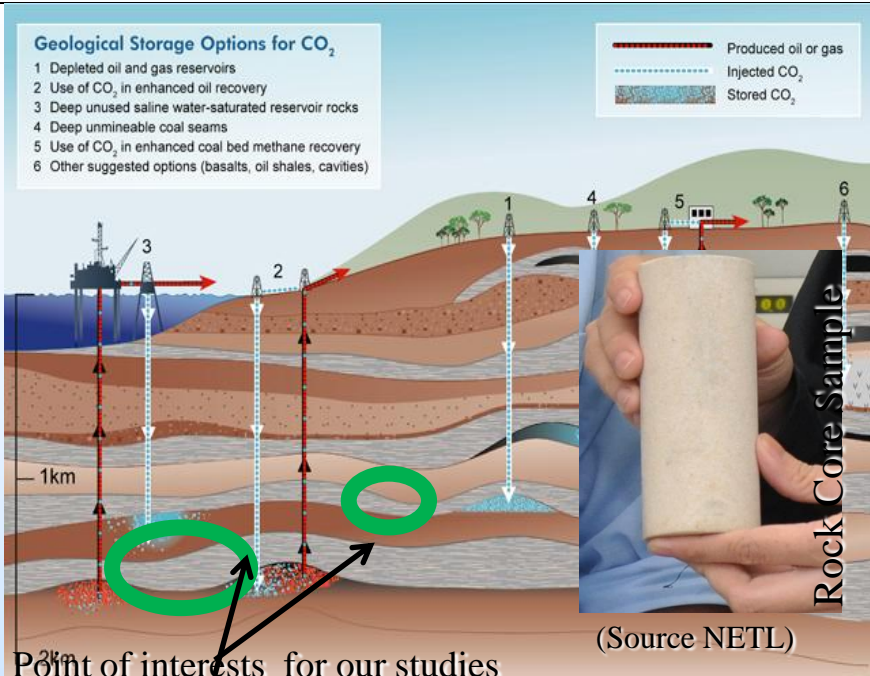
- Develop a computational technique to estimate fluid conductance.
- Investigate the capillary effects at pore-scale to determine the on CO<sub>2</sub> sequestration kinetics and storage capacity.
- Develop a framework for coupled system of micro-scale (pore-scale) physics with macro-scale (a reservoir scale) physics.

# Technical Status

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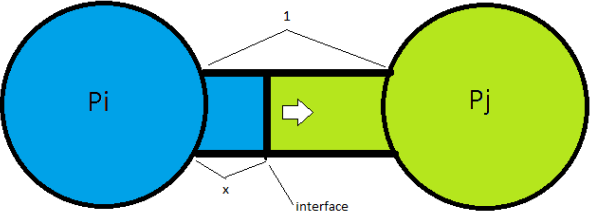
- Pore-network modeling
- Conductance derivation for irregular geometry
- Pore-to-CFD Computations
- Paul M. Delgado's presentation "*Stochastic Multiscale Modeling of Fluid Flow in Porous Media for CO2 Storage Applications*"

# Pore-network construction





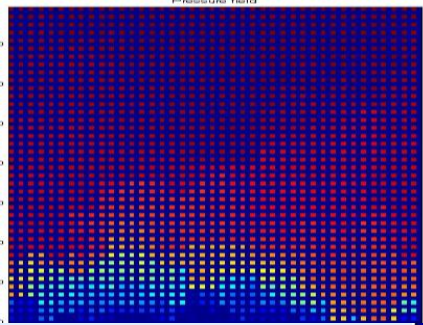
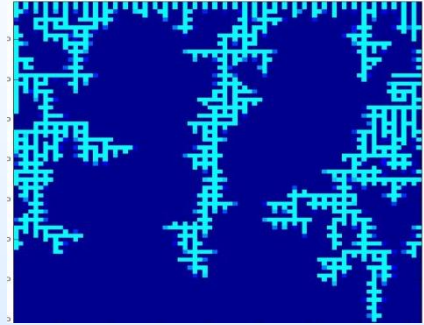
# Pore-network modeling



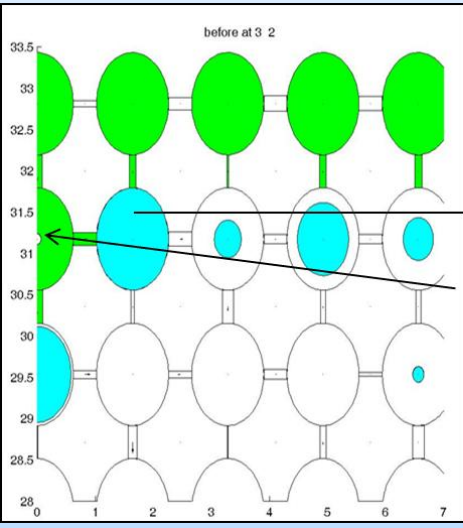
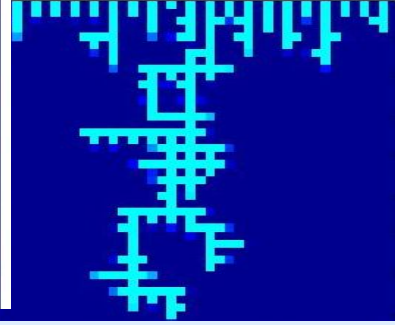
$$q_{ij} = g_{ij} \nabla P_{ij} \quad \sum_{j \in K_i} q_{ij} = 0$$

$$g = \frac{1}{8(x\mu_{inv} + (1-x)\mu_{def})L}$$

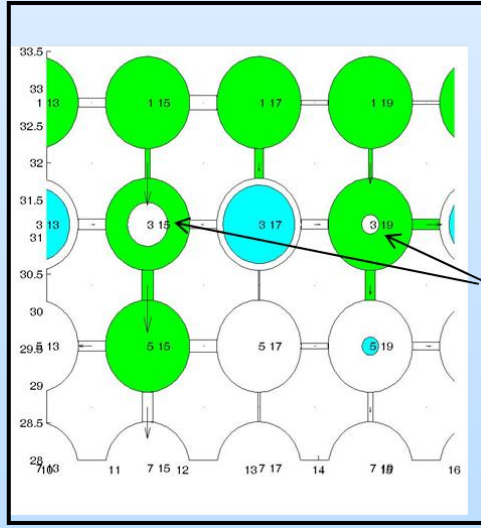
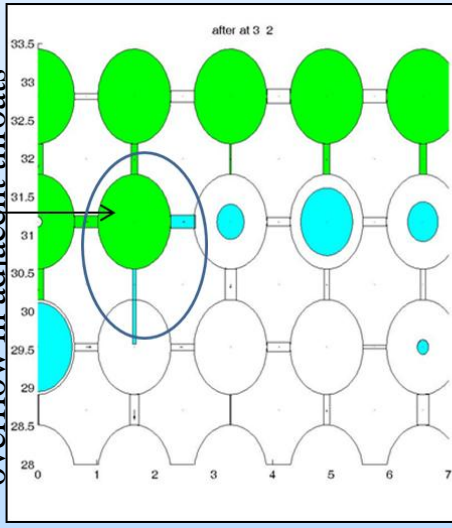
Saturation and Pressure profiles



Constant injection



Overflow in pore produces overflow in adjacent throats

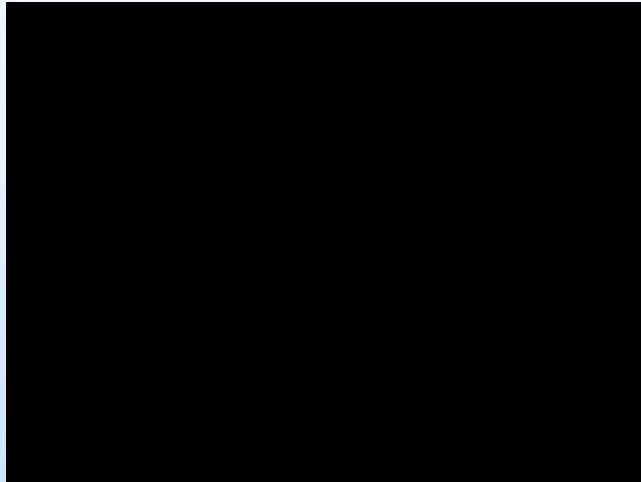


Address backflow with Artificial reservoir

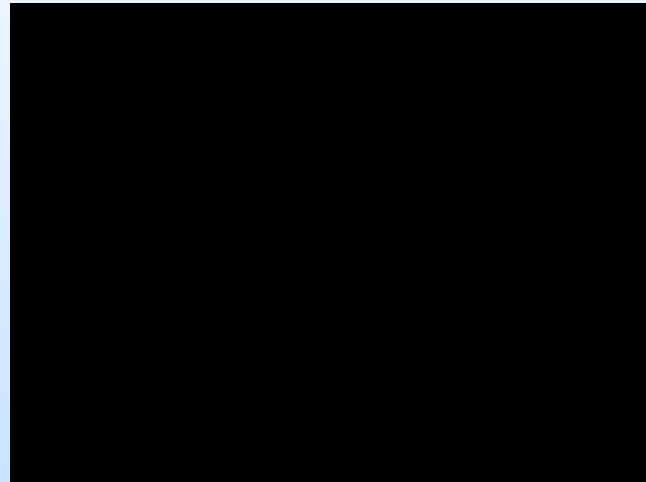
# Pore-network modeling

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[Video 1](#)

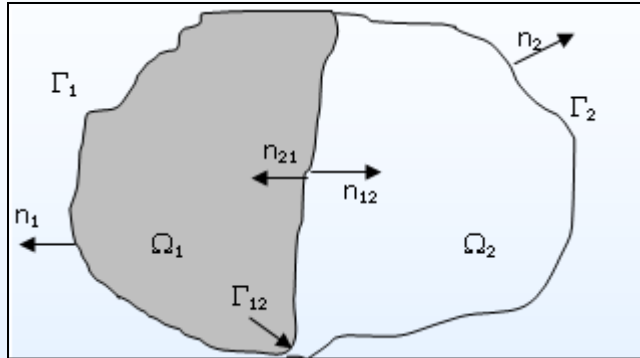


[Video 2](#)





# Variational Formulations



*Express solution of Stokes equation in terms of the minimization of a functional  $I[f]$  (meaning just an integral of a function of  $f$  and its derivatives over the flow domain). Most treatments start by considering the one-dimensional case*

The fluid velocities  $w_1(x, y)$  and  $w_2(x, y)$  satisfy

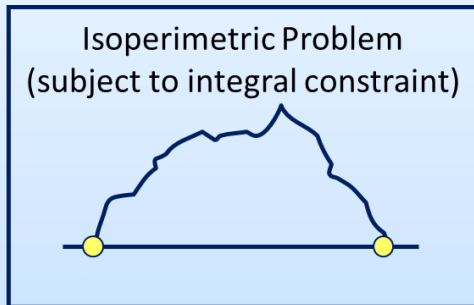
$$\nabla^2 w_i = -\frac{G_i}{\mu_i} \quad \text{on } (x, y) \in \Omega_i$$

BCs:  $w_i(x, y) = 0$  on  $(x, y) \in \Gamma_i = 0$

$$w_1(x, y) = w_2(x, y), \&$$

$$\mu_1 \mathbf{n}_{12} \cdot \nabla w_1(x, y) = \mu_2 \mathbf{n}_{21} \cdot \nabla w_2(x, y) = 0 \quad \text{on } (x, y) \in \Gamma_{12}$$

Introduce a functional  $I[f_1, f_2]$  such that  $f_i$  is any  $C_2$ -regular function vanishing on  $\Gamma_i$  and  $f_1 = f_2$  on  $\Gamma_{12}$ .



# Variational Formulations

Fluxes:  $q_i = \int_{\Omega_i} w_i dx dy$

Minimization of the functional results in

$$I[f_1, f_2] = \frac{1}{2} \int_{R_1} dx dy \left[ \mu_1 \nabla f_1 \cdot \nabla f_1 - 2G_1 f_1 \right] + \frac{1}{2} \int_{R_2} dx dy \left[ \mu_2 \nabla f_2 \cdot \nabla f_2 - 2G_2 f_2 \right]$$

$$I[f_1, f_2] \geq I[w_1, w_2] \text{ with equality if and only if } f_1 = w_1 \text{ and } f_2 = w_2$$

In fact, we show

$$I[f_1, f_2] - I[w_1, w_2] =$$

$$\frac{1}{2} \int_{R_1} dx dy \mu_1 \nabla (f_1 - w_1) \cdot \nabla (f_1 - w_1) + \frac{1}{2} \int_{R_2} dx dy \mu_2 \nabla (f_2 - w_2) \cdot \nabla (f_2 - w_2)$$

Now

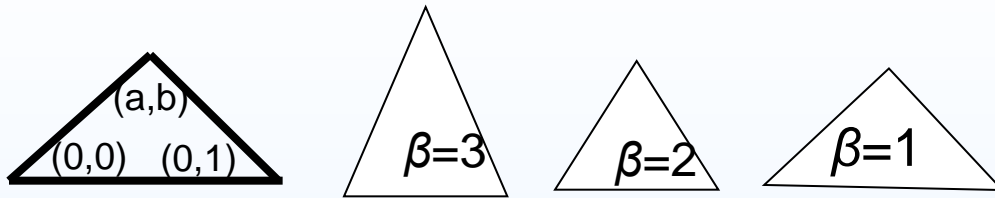
$$\mu_i \nabla (f_i - w_i) \cdot \nabla (f_i - w_i) = \mu_i \left[ \nabla f_i \cdot \nabla f_i - 2 \nabla w_i \cdot \nabla f_i + \nabla w_i \cdot \nabla w_i \right]$$

$$= \mu_i \left[ \nabla f_i \cdot \nabla f_i - \nabla w_i \cdot \nabla w_i - 2 \nabla w_i \cdot \nabla (f_i - w_i) \right]$$

$$= \mu_i \left[ \nabla f_i \cdot \nabla f_i - \nabla w_i \cdot \nabla w_i - 2 \nabla \cdot \left[ \nabla w_i (f_i - w_i) \right] + 2 \nabla^2 w_i (f_i - w_i) \right]$$

$$= \mu_i \left[ \nabla f_i \cdot \nabla f_i - 2(G_i / \mu_i) f_i - \nabla w_i \cdot \nabla w_i - 2(G_i / \mu_i) w_i \right] + 2 \nabla \cdot \left[ \nabla w_i (f_i - w_i) \right]$$

# Flow Conductance Derivation



$$a = \frac{1}{2}, \beta' = \beta, \Rightarrow g = \frac{\beta^3}{160(3 + \beta^2)}$$

$$g_{emp} = 0.6 \frac{(area)^3}{(perimeter)^2} = \frac{3\beta^3}{320(1 + \sqrt{1 + \beta^2})^2}$$

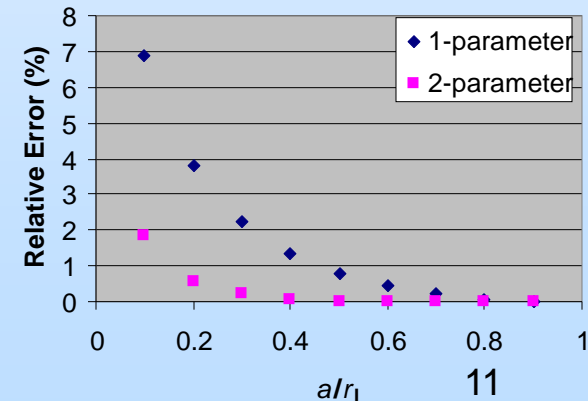
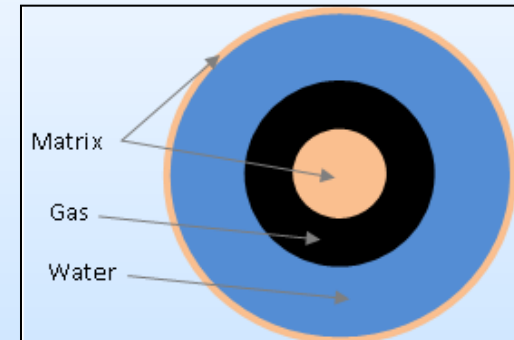
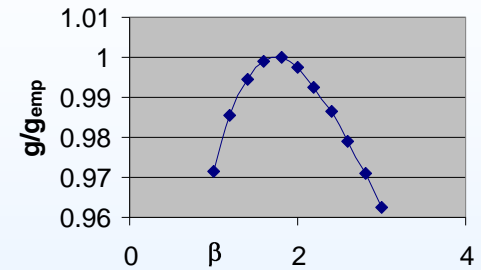
Annular flow:  $a < r < 1$ ,  $G/\mu = 1$

$$\text{Exact solution: } w = \frac{1}{4}(1 - r^2) - \frac{(1 - a^2)}{\ln(\frac{1}{a})} \ln\left(\frac{1}{r}\right)$$

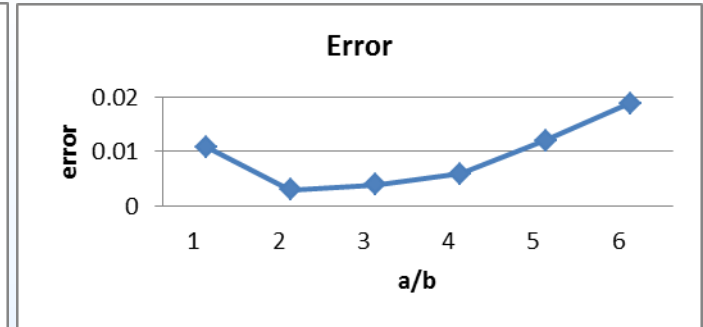
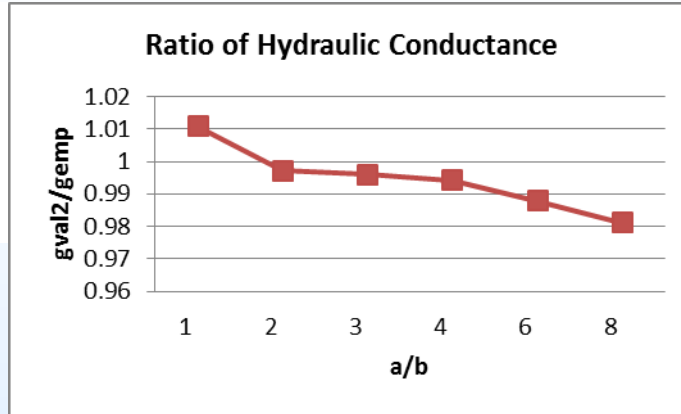
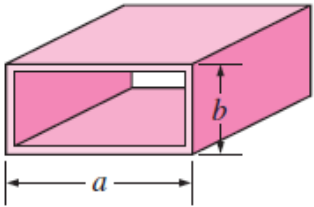
1&2 parameter choices for f:

$$f = \alpha(1 - r)(r - a)$$

$$f = (1 - r)\{\alpha(r - a) + \beta(1 - a^2)\}$$



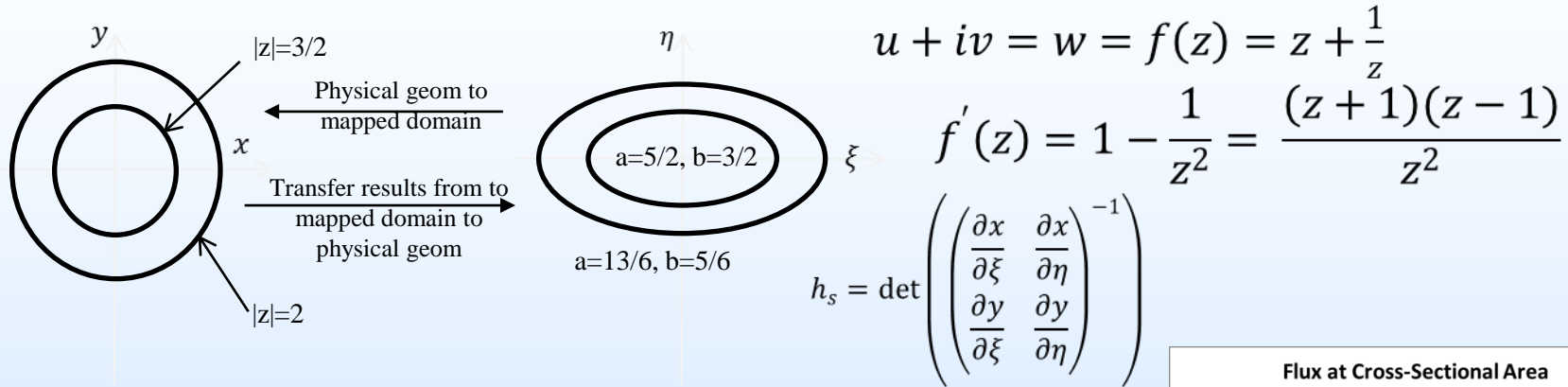
# Flow Conductance Derivation



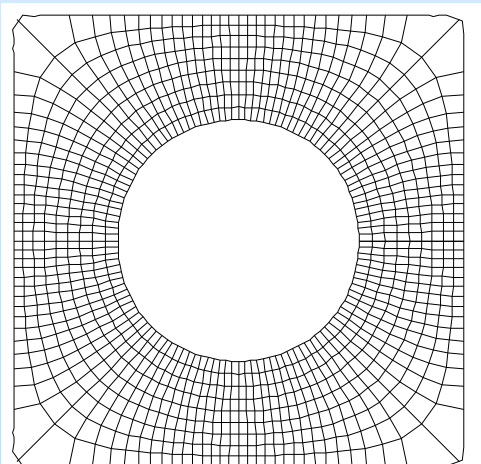
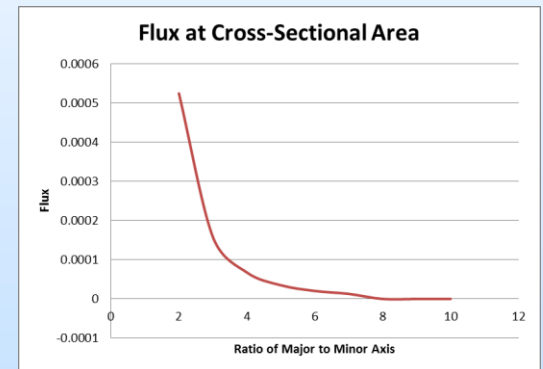
r	Flow resistance factor		
	f	$f_{val1}$	$f_{val2}$
1	56.92/Re	57.6/Re	56.9829/Re
1.5	N/A	59.904/Re	58.9759/Re
2	62.20/Re	64.0/Re	62.3823/Re
2.5	N/A	68.1796/Re	65.7029/Re
3	68.36/Re	72.0/Re	68.6318/Re
4	72.92/Re	78.336/Re	73.3537/Re
5	N/A	83.2/Re	76.9438/Re
6	78.80/Re	86.9878/Re	79.7622/Re
7	N/A	90/Re	82.035/Re
8	82.32/Re	92.4444/Re	83.9067/Re
10	N/A	96.1587/Re	86.8061/Re
15	N/A	101.7/Re	91.2704/Re
20	N/A	104.751/Re	93.8025/Re

r	Hydraulic Conductance, g		$\frac{g_{val2}}{g_{emp}}$	Er
	$g_{emp}$	$g_{val2}$		
1	0.0347222	0.0350983	1.0108	0.01083
1.5	N/A	0.0732503	N/A	N/A
2	0.114327	0.113992	0.997078	0.00292
2.5	N/A	0.155306	N/A	N/A
3	0.197484	0.196702	0.99604	0.00396
4	0.280856	0.279195	0.994088	0.00591
5	N/A	0.361014	N/A	N/A
6	0.447529	0.44213	0.987936	0.01206
7	N/A	0.522643	N/A	N/A
8	0.614285	0.602668	0.98109	0.01891
10	N/A	0.761648	N/A	N/A
15	N/A	1.15556	N/A	N/A
20	N/A	1.54713	N/A	N/A

# Flow Conductance – Conformal Mapping



$$q = \int f dA = \int f(\xi, \eta) h_s d\xi d\eta,$$



Modified Schwarz-Christoffel Transformations

$$f(z) = A \int^z \prod_{j=1}^n (z' - z_j)^{(\alpha_j - 1)} dz' + B$$

# Pore-to-CFD

Raw CT Scan

Segmentation

3D Reconstruction

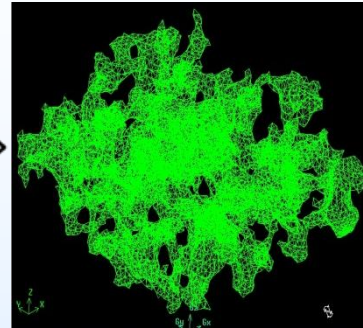
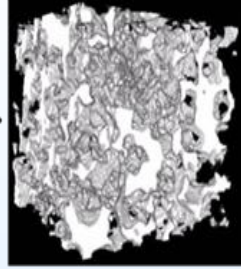
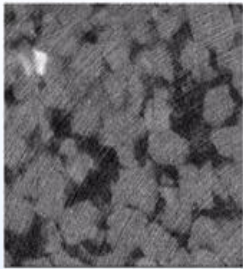
CFD Mesh:

4,321,166 elements

924,426 nodes

Duration for meshing 24-48 hrs

Software used: Gambit



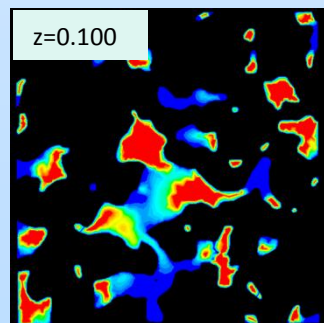
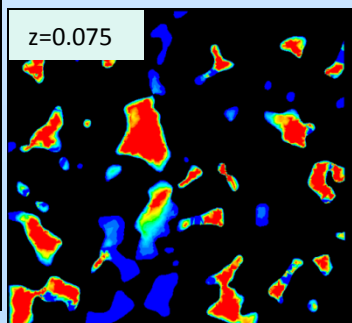
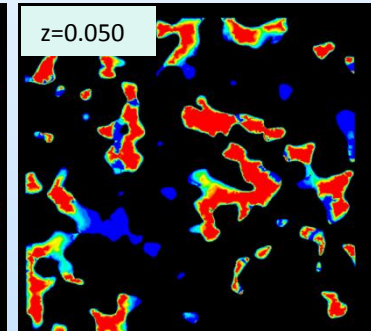
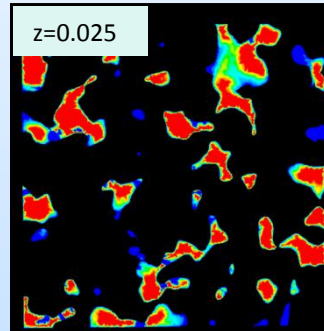
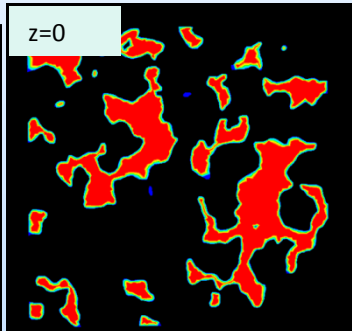
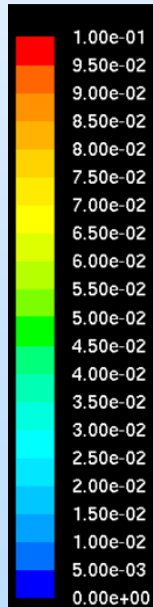
Courtesy: B.Lindquist, SUNY

Preprocessing

Connected Volume

Maximal  $f$

Extraction



Velocity profile

# Accomplishments to Date

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- Developed conductance model for irregular pore-cross section using conformal mapping
- Created pore-network reconstruction for CT-scanned images from NETL and Examined the flow kinetics of flow using CFD
- Addressed the convergence issues associated with the backflow in the pore-network model obtained from the NETL
- Devised a framework for coupling micro-scale with macro-scale
- Developed non-Newtonian flow models using variational calculus approach



# Summary

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- Key Findings
  - Variational methods seem a promising way of obtaining approximate analytical expressions for hydraulic conductance of pore elements for input into pore network models
  - Resolved backflow issues using virtual storage
- Lessons Learned
  - Micro- to macro-scale coupling is not so straightforward due to significant orders of scale differences
  - Pore network has numerical convergence issues
- Future Plans
  - Micro-scale (pore-scale) to macro-scale (Reservoir scale)
  - Develop advance linear algebra-solver
  - High Performance Computing

# Appendix

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- Organization Chart
- Gantt Chart
- Bibliography

# Organization Chart

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Principal Investigator: Dr. Vinod Kumar  
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Tel: 915-747-6075; Fax 915-747-5019,  
E-mail: [vkumar@utep.edu](mailto:vkumar@utep.edu)

# Organization Chart

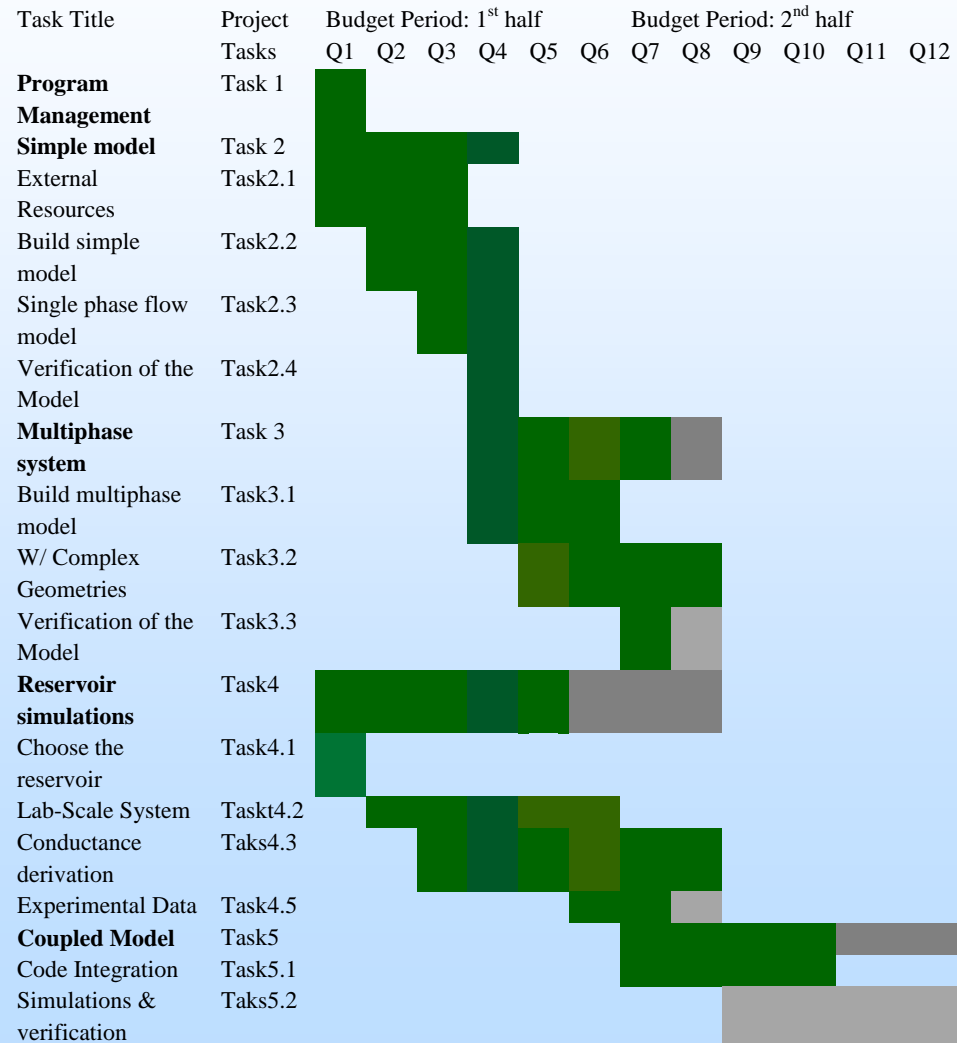
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## Students participants:

- Mr. P. Delgado, Doctoral, Computational Science & Engineering
- Ms. Fan Chen, Doctoral, Computational Science & Engineering
- Mr. Todd Dorethy, M.S., Computational Science & Engineering
- Mr. N. Kavoori, M.S., Mechanical Engineering (Graduated, 2010)
- Other students who partially supported us on this project:
  - Dr. K. Katta (Computational Science),
  - Mr. Enrique Busquestes (BS, Mechanical)
  - Mr. R. Chacon (BS, Mechanical)
  - Mr. E. Cordero (BS, Mechanical),
  - Mr. J. Ortega (BS, Mechanical),
  - Ms. S. Afrin (MS, Mechanical),
  - Mr. D. Llauhas (BS, Mechanical),
  - Mr. D. Landis (Computational Science),
  - Mr. G. Aceves (Mechanical)

*Note: This project also enabled Mr. P. Delgado to get the NSF's LSAMP Scholarship for his continuation of doctoral studies and helped the PI to acquire funding from Student Employment Program (provided by the university from a funding from the state of Texas*

# Gantt Chart



# Bibliography

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